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Insight into the mechanism of catalytic combustion of acrylonitrile over Cu-doped perovskites by an experimental and theoretical study



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ABSTRACT

A series of LaFeO₃, La₂Cu₂O₄, and Cu-doped perovskite-typed LaB_{0.8}Cu_{0.2}O₃ (B = Fe, Co, and Mn) catalysts were studied for the selective catalytic combustion of acrylonitrile (C2H3CN). The physicochemical properties of these materials were characterized by XRD, N₂ sorption, H₂-TPR, and XPS, thereafter correlating to their diverse evolutions of N2 yield. The best performance was achieved over the LaFe_{0.8}Cu_{0.2}O₃ sample owing to an easy transformation from Cu²⁺ to Cu⁰ at low temperatures. Moreover, the mechanism on selective catalytic combustion of acrylonitrile over LaFeO3 and LaFe08 Cu02O3 was investigated by in-situ DRIFTs and density functional theory (DFT) calculations. It has been noted that malonic acid species were generated on the surface of LaFe_{0.8}Cu_{0.2}O₃ sample and the acrylic species steadily existed over LaFeO₃, indicating that the strongly oxidative copper ion promotes an oxidation of C-terminal to carboxylic acid species at low temperatures. In addition, the copper substitution into LaFeO3 can greatly reduce energy barrier for the transformation from -NH-O to -N-OH, which is thought as the rate-determining step for N2 formation. In summary, the catalytic combustion of acrylonitrile commonly follows an oxidationdominate mechanism over LaFe_{0.8}Cu_{0.2}O₃, whereas fulfills with a hydrolysis-dominate mechanism over LaFeO₃. 5% H₂O addition into the feed caused a slightly and reversible decrease in N₂ yield as well as an improved NO production, while a poisoning by 100 ppm SO₂ was found due to serious coverage of active centers by sulfurous species.

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1. Introduction

The purification of nitrile emissions coming from acrylonitrile (CH₂=CH−C≡N) production becomes more and more urgent and significant due to its intensively carcinogenic properties which lead to serious environmental and human health problems. Incineration is a simple method to remove this nitrile gas, but the related process is normally operated at high temperatures (around 800 °C), which needs additional fuel consumption. More importantly, direct incineration might lead to the formation of a large number of byproduct such as nitrogen oxides (NO_x), which causes a secondary pollution. Conversely, catalytic combustion of acrylonitrile has been widely studied owing to the relatively lower operation temperature and its excellent performances especially high N₂ and CO₂ selectivity. Therefore, exploring the effective catalytic material which has good catalytic activity for acrylonitrile removal and high selectivity of the targeted products (N2 and CO2) is particularly necessary. Gervasini et al. studied that the synergic effects of Ba-CuO-Cr₂O₃/Al₂O₃ catalyst associated with ozone which was used as strong oxidant during acrylonitrile combustion [1]. However, this work only focused on the acrylonitrile conversion but ignored the N2 selectivity. Nanba et al. [2,3] demonstrated Ag was an efficient catalyst for acrylonitrile decomposition and explored the effect of different support materials as well as indentified the oxidation state of Ag. Besides, zeolite-supported transition-metals were also reported to show excellent performances for nitrile combustion [4–7]. Cu-ZSM-5 completely converted acrylonitrile with an N₂ selectivity of 80% or more at >350 °C. The redox property between Cu²⁺ and Cu⁺ is reported to be responsible for combustion activity [6,7]. In addition, Poignant et al. [8] proposed a mechanism that acrylonitrile adsorbed on Cu⁺ decomposed rapidly into ethylene and cyanide (Cu^+CN) during the selective catalytic reduction of NO_x by propane. Anyhow, Cu species over zeolites could effectively promote the decomposition activity of acrylonitrile and improve N₂ selectivity at a relatively low temperature. However, few manuscripts, involving selective catalytic combustion of nitrile by the mixed oxides, especially perovskite-type oxides with their unique structure and versatility of compositions, have been reported in recent years.

Perovskites are described by a general ABO₃ formula, which have been proposed to be potential substitutes of noble metals

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being a redox catalyst [9]. In the perovskite structure, A cation can be a lanthanide or alkaline-earth cation, while B cation is a transition-metal element which is commonly believed to serve as the active sites in environmental catalytic reaction [10,11]. These materials commonly show satisfactory activities not only in the complete oxidation system such as CO [12,13], CH₄ [14], VOCs [15,16] etc., but also in the selective catalytic reduction (SCR) of NO system. Diverse reductants such as C₃H₆ [17–20] and NH₃ [21] were applied for the NO-SCR processes. Both Zhang [20] and Yang [22] have demonstrated that SCR performance along with N₂ selectivity is improved by an incorporation of Cu²⁺ into the lattice of perovskites. In the process of mechanism research, some important intermediates such as -CN and adsorbed (CN)₂ yielding during the SCR of NO are also the initial adspecies during the catalytic combustion of acrylonitrile [22]. A similar result that acrylonitrile has been regarded as a possible intermediate to form N₂ was also studied by Nanba et al. [8]. Therefore, there is reason to think that these perovskite-type materials, especially doped by Cu²⁺, would show promising performances in the catalytic combustion of acrylonitrile. Aiming at developing an industrial catalyst, special attention should be paid for the influence of steam on catalytic performance because large amount of water vapor would be generated during this combustion process. The resistance towards SO₂ poisoning also needs to be considered although acrylonitrile production generally belongs to a low-contamination process.

In the present study, LaB_{0.8}Cu_{0.2}O₃ (B=Fe, Co, and Mn) was synthesized by citrate complexation procedure and further characterized by N2 physisorption, X-ray diffraction (XRD), H2temperature programmed reduction (TPR) and X-ray spectroscopy (XPS). *In-situ* diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) was performed for a better understanding of reaction mechanism for acrylonitrile catalytic combustion occurring over LaFeO₃ and LaFe_{0.8}Cu_{0.2}O₃ as well as how the Cu²⁺ ions promote activity of acrylonitrile elimination and improve N₂ selectivity. The reaction paths of acrylonitrile oxidation, including the free energy of intermediates and transition states, were analyzed by density functional theory (DFT) calculations in order to clarify the details of bond formation and fracture of the corresponding intermediates species. Ultimately, a deep insight into mechanism of catalytic combustion of acrylonitrile to generate N₂ and CO₂, combining in-situ DRIFTs investigations with DFT calculations, over Fe-based perovskite doped by Cu²⁺ was herein represented. The influence of water vapor and sulfur dioxide on combustion performances was also addressed.

2. Experimental

2.1. Catalyst preparation

A series of perovskite catalysts with different B-site cations (B=Fe, Co, and Mn) partially substituted by Cu²⁺ was synthesized by the classical citrate complexation [21,23] (see details in Section S1 of Catalysts preparation in SI).

2.2. Characterization

These perovskite catalysts were characterized by several techniques including XRD, N₂ sorption, H₂-TPR, and XPS, with details being addressed in Section S2 of Characterization in SI.

2.3. Catalytic activity measurements

The catalytic combustion of acrylonitrile was performed in a quartz fixed-bed reactor (i.d. = 0.6 cm, L = 40 cm) under an atmosphere of 3000 ppm acrylonitrile and 1.6 vol% O₂, balanced by He

with a space velocity of approximate $120,000 \, h^{-1}$. The whole reaction pipeline was thermally insulated at $100\,^{\circ}\text{C}$ with heating tape. The water and sulfur resistance tests were also performed in a quartz fixed-bed reactor with H_2O and SO_2 being simultaneously introduced under space velocity of about $120,000 \, h^{-1}$. The experimental facilities are described in Section S3 of Catalytic activity measurements in SI.

2.4. In-situ DRIFTS study

In-situ diffuse reflectance infrared Fourier-transform spectroscopy (DRIFTS) was performed to investigate the surface absorbed species upon temperature. The concentrations of acrylonitrile and $\rm O_2$ in the gas mixture were 1.2 vol% and 6.4 vol%, respectively, with He as the balance gas, and the total flow rate was 60 ml/min. The in-situ DRIFTS equipment and experimental method are presented in Section S4 of In-situ DRIFTS study in SI.

2.5. Computational methods

All of the calculations were performed with the density functional theory (DFT) provided by the program DMol3 package [24]. Spin-polarized calculations were employed using the generalized gradient approximation (GGA) with the Perdew-Burke-Ernzerhof (PBE) method to describe the exchange and correlation energy in all calculations. For calculations of geometry optimization, a $1\times3\times1$ Mon-Khorst-Pack k-point mesh for the Brillouin zone sampling was used. Using periodic boundary, a plane-wave cutoff energy of 400 eV has been employed throughout. The LaFeO₃ crystal with an orthorhombic perovskite structure [Pnma (62)] was calculated with 28 atoms in the unit cell. We explore both possibilities using a supercell ($1\times2\times1$), slab model of the LaFeO₃ and LaFe_{1-x}Cu_xO₃ perovskite terminated upon the most common, (0 1 0) facet of the material [25,26].

The energy of adsorption, E_{ads} , for the acrylonitrile molecules on the surface is defined as:

$$E_{ads} = E_{adsorbate + surface} - E_{surface} - E_{gas}$$

where $E_{surface}$ is the total clean relaxation energy of the surface slab, E_{gas} is the energy of the gas-phase adsorbate, and $E_{adsorbate+surface}$ is the total energy of the composite system. Since the calculations are performed at 0 K and fixed cell volume, the differences in Gibbs free energy should equal the differences in total energy. By this definition, a negative value of E_{ads} corresponds to an exothermic and spontaneous adsorption process.

To locate saddle points and calculate the reaction pathway, the climbing image-the nudged elastic band (CI-NEB) method was used [27]. This is a "chain of states" method, where several intermediate states or images of the system are connected by springs to map out a reaction pathway between the initial and final states.

3. Results and discussion

3.1. Physicochemical properties

XRD patterns of the perovskite-type materials (LaFeO₃, LaFe_{0.8}Cu_{0.2}O₃, LaCo_{0.8}Cu_{0.2}O₃, LaMn_{0.8}Cu_{0.2}O₃, and La₂CuO₄) are illustrated in Fig. S1. All five as-prepared samples show pure perovskite structure, but the locations of diffraction peaks of these perovskite-type samples are slightly different, which result from the distinction of B-site metals. Furthermore, no diffraction line corresponding to external CuO or Cu₂O can be detected, suggesting that Cu is successfully incorporated into the perovskite lattice. Moreover, specific surface area (15–40 m²/g) determined by N₂

sorption and crystallite size (10–25 nm) calculated by Scherrer equation, are listed in Table S1.

H₂-TPR profiles for different perovskites with and without Cudoping are shown in Fig. S2, which is mainly used to investigate the influence of Cu substitution on the related redox abilities. The location and assignment of reduction peaks of as-prepared samples were detailedly discussed in Section S6 of Redox properties in SI. Seeing from Fig. S2, a large peak at 292 °C appearing in the case of La_2CuO_4 can be attributed to the reduction of Cu^{2+} to Cu^0 , whereas a small peak at 546 °C may be possibly ascribed to the reduction of bulk CuO to Cu⁰ [28]. There is no obvious reduction peak observed for LaFeO₃ in comparison with La₂CuO₄, indicating the limited redox ability of the former. Actually, LaFeO3 was verified to be hardly reducible up to 700 °C [22,29]. The quantitative calculation of H₂ consumption and cation reduction percentage are described in Table S2. For all the Cu-doped samples, Cu being incorporated into the lattice of perovskites not only improved the redox ability at low temperatures but also facilitated the corresponding reduction percentages, for Co^{3+} from 73.0% to 98.6%, for Mn^{2+} from 66.7% to 79.2%, and for Fe^{3+} from 4.0% to 10.4%, as depicted in Table S2, which might effectively promote catalytic combustion of acrylonitrile.

XPS of O1s and Cu $2p_{3/2}$ for LaFe_{0.8}Cu_{0.2}O₃, LaCo_{0.8}Cu_{0.2}O₃, and LaMn_{0.8}Cu_{0.2}O₃ samples are profiled in Fig. S3a and S3b with the related quantitative analyses being simultaneously conducted in Section S7 of Surface element study in SI. The surface components of atomic La, M (M=Fe, Co, Mn, Cu), and O derived from XPS are listed in Table S3. It can be found that LaFe_{0.8}Cu_{0.2}O₃ possessed the comparatively low contents of surface atomic Cu (2.06%) but presented the highest Cu²⁺/Cu⁺ ratio. This result suggests that Fe-O-Cu structure is inclined to expose high valence of Cu. On one hand, LaFe_{0.8}Cu_{0.2}O₃ provided the lowest O_{ads}/O_{lat} atomic ratio (1.31) among the Cu-doped samples which might benefit for inhibiting the excessive oxidation of nitrogen atom into the higher N-valence products like N₂O, NO, and NO₂. On the other hand, the O_{ads}/O_{lat} of $LaFe_{0.8}Cu_{0.2}O_3$ (1.31) is much higher than that of $LaFeO_3$ (0.67), which is mainly due to the increase of oxygen vacancy due to Cu substitution. The high density of anionic oxygen vacancy on LaFe_{0.8}Cu_{0.2}O₃ was believed to be favorable for the adsorption and activation of O2 [30], and hence enhancing catalytic activity for acrylonitrile combustion.

3.2. Activity test

The temperature dependence on the conversion of acrylonitrile as well as the yields of N-containing products (N2, NH3, N2O, NO, NO₂) and C-containing products (CO₂, CO) during nitrile combustion over LaFeO₃ and LaB_{0.8}Cu_{0.2}O₃ (B=Fe, Co, and Mn) samples are depicted in Fig. 1a-d. As presenting in Fig. 1a, the initial activity is achieved at 200 °C for pure LaFeO₃ perovskite and at 150 °C for Cu-doped samples, acrylonitrile conversion occurring over pure LaFeO₃ is gradually increased upon temperature and reach 100% at 400 °C; however, Cu substitution could prompt the temperature reduce to 250 °C for a complete acrylonitrile conversion and the Coand Mn-based perovskite doped by Cu can also achieve this effect. It demonstrates that the perovskite-type materials commonly show excellent activities for catalytic removal of acrylonitrile even at low temperatures. Apart from acrylonitrile conversion being a crucial indicator for evaluating the combustion performances, N₂ and CO₂ yields constituting other criterions are also important due to the possible releasing of toxic byproducts (NH₃, NO, N₂O, NO₂, and CO) during acrylonitrile combustion. As shown in Fig. 1a, N2 yield of $LaFe_{0.8}Cu_{0.2}O_3$ is apparently higher than those of the other samples at temperatures above 300 °C (around 80%). It has been found that an enhancement in N₂ yield at T < 400 °C for LaFe_{0.8}Cu_{0.2}O₃ was likely caused by Cu²⁺ substitution improve its redox ability at

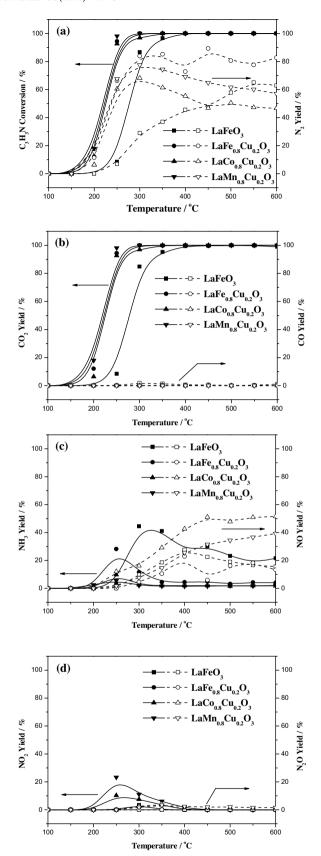


Fig. 1. Catalytic performance as a function of temperature during acrylonitrile combustion over LaFeO₃ and LaB_{0.8}Cu_{0.2}O₃ (B=Fe, Co, and Mn) samples: (a) acrylonitrile conversion and N₂ yield; (b) CO₂ and CO yield; (c) NH₃ and NO yield; (d) N₂O and NO₂ yield. Conditions: 3000 ppm AN, 1.6 vol% O₂, and GHSV = 120,000 h⁻¹.

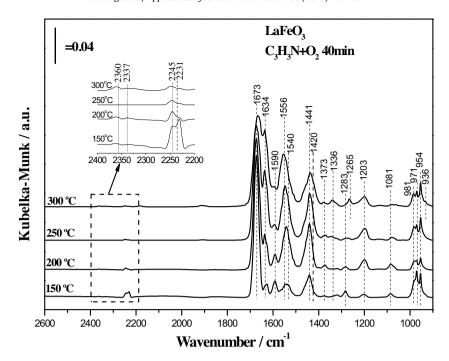


Fig. 2. DRIFT spectra of LaFeO3 with an exposure to 1.2 vol% acrylonitrile, 6.4 vol% O2, with He to be the balance gas in the range of 150-300 °C.

low temperatures. The existence of Fe-O-Cu structure in the lattice of perovskite could benefit to generate N2 in the SCR of NO reaction, which was demonstrated by the previous reports [18,22]. While at the high temperatures from 400 °C to 600 °C, the oxidation property of Fe becomes weaker than those of Mn and Co, according to H2-TPR results, which leads LaFe_{0.8}Cu_{0.2}O₃ to produce more N_2 as well as $LaMn_{0.8}Cu_{0.2}O_3$ and $LaCo_{0.8}Cu_{0.2}O_3$ to produce large amount of undesirable NO_x byproducts. The profiles of CO₂ and CO yields depicted in Fig. 1b show that carbonaceous species, in the presence of excessive O2, are directly oxidized to CO₂ over these three samples, which indicates that CO₂ generation is only related to O2 concentration and hardly affected by perovskite compositions. The yields of N-containing byproducts (NH₃ and NO) and (N₂O and NO₂) are respectively illustrated in Fig. 1c and d, which are helpful to understand the trails of nitrogen except generating N2. As seen from Fig. 1c and d, NH3 and N₂O with relatively lower N valences are usually yielded at low temperatures from 150 to 400°C, associated with an order of $LaFe_{0.8}Cu_{0.2}O_3 > LaCo_{0.8}Cu_{0.2}O_3 > LaMn_{0.8}Cu_{0.2}O_3$ for NH₃ yield and an order of LaMn_{0.8}Cu_{0.2}O₃ > LaCo_{0.8}Cu_{0.2}O₃ > LaFe_{0.8}Cu_{0.2}O₃ for N2O yield. This finding indicates that mechanism for acrylonitrile catalytic combustion over these samples may vary from one to another. For LaFe_{0.8}Cu_{0.2}O₃ sample, due to the large generation of N₂ accompanying with certain amount of NH₃, it is speculated that NH₃ is an important intermediate during the reaction. Based on above analyses, it is realized that LaFe_{0.8}Cu_{0.2}O₃ not only possessing higher acrylonitrile activity but also exhibiting the best selectivity toward N2 and CO2 is a promising candidate as a catalyst for acrylonitrile selective combustion.

3.3. Mechanism study based on DRIFTS

The mechanism of catalytic combustion of acrylonitrile over different types of catalyst has been investigated [2,3,7]. Basically, two main mechanisms can be distinguished: hydrolysis mechanism in which acylamino (—CONH₂) was formed through nitrile (—CN) hydrolysis over Fe/SBA-15 and oxidation mechanism in which the isocyanate (–NCO) could be generated over Cu/SBA-15 through an

oxidation of nitrile (-CN) [5,31]. Nanba et al. [7] also demonstrated that acrylonitrile was mostly converted to isocyanate (-NCO) over Cu/ZSM-5, indicating that it tends to follow oxidation mechanism in the presence of copper species. However, the acrylonitrile catalytic combustion reaction mechanism over perovskites has so far not been studied.

3.3.1. In-situ DRIFTs of catalytic combustion of acrylonitrile over $LaFeO_3$

LaFeO₃ perovskite shows certain reactivity for acrylonitrile combustion, while Cu substitution (LaFe_{0.8}Cu_{0.2}O₃) not only lowers the temperature for acrylonitrile complete conversion by 100 °C but also greatly improves the N2 yield up to 80% at high temperature (above 300 °C). In order to sufficiently understand the surface reaction mechanism influenced by Cu substitution, the related mechanisms conducting over LaFeO₃ and LaFe_{0.8}Cu_{0.2}O₃ perovskites are investigated via in-situ DRIFTS study conducted at different temperatures. The contradistinction of acrylonitrile catalytic conversion between these two samples was explored with an emphasis on the formation of diverse intermediates due to Cu substitution. Fig. 2 shows IR spectra during an exposure of LaFeO₃ perovskite to gas mixture containing 1.2 vol.% acrylonitrile, 6.4 vol.% O₂, with He balance gas in a temperature range of 150-300 °C. Each curve depicts a change of surface species after reactant gas is fed at corresponding temperatures for 40 min. The band at 971 cm⁻¹ attributed to bending vibration of C—H of gaseous acrylonitrile is clearly observed. Additionally, the bands at 2231 and 2245 cm⁻¹ were also detected at 150 °C attributed to the C≡N functional group in acrylonitrile, implying that acrylonitrile was adsorbed upon LaFeO₃ through N-terminal adsorption. The adsorption process is described as Eq. (1), in which solid line represents a coordinate or ionic bond (respectively for adspecies or perovskite):

The intensity of these peaks was significantly reduced along with the rise of temperature. At $T=300\,^{\circ}\text{C}$, only small amounts

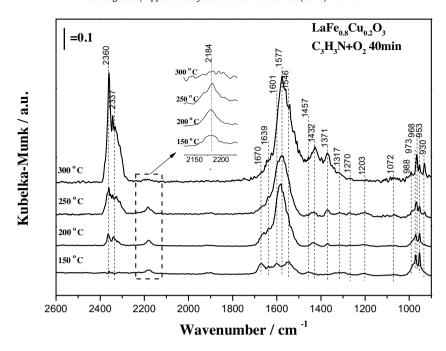


Fig. 3. DRIFT spectra of LaFe_{0.8}Cu_{0.2}O₃ with an exposure to 1.2 vol% acrylonitrile, 6.4 vol% O₂, with He to be the balance gas in the range of 150-300 °C.

of —CN groups are remained, suggesting that —CN fragment was mostly converted into other species upon the increasing temperature. According to the literature reports [2,7], the bands exhibited at 1203, 1540, 1590, and 1673 cm⁻¹ were assigned to the adsorbed acrylamide species, among which the band at 1673 cm⁻¹ represented the C=C vibrations [ν (C=C)] of acrylamide and the weak bands at 1203 and 1590 cm⁻¹ correspond to the asymmetric deformation of NH₃ [δ _{as}(NH₃)] coordinated to Lewis acid sites [32,33]. Besides, the synergy of N—H bending vibration and C-N stretching vibration generates a small band at 1540 cm⁻¹. All the evidences strongly demonstrated that acrylonitrile was easily hydrolyzed to generate acrylamide over Fe-based catalyst at relatively low temperatures, as formulated by Eq. (2):

$$CH_{2}=CH \qquad CH_{2}=CH \qquad NH_{2}$$

$$Fe^{3+} \qquad Fe^{3+} \qquad + \qquad H_{2}O \qquad Fe^{3+} \qquad Fe^{3+}$$

$$O^{2-} \qquad O^{2-} \qquad (2)$$

Simultaneously, the bands at 1081, 1373, 1441, 1556, and 1634 cm⁻¹ were also detected and attributed to acrylic acid species produced by the further hydrolysis of adsorbed acrylamide species according to the literature [2,34]. The bands at 1441 and 1540 cm⁻¹ were assigned to $v_{as}(COO^-)$ and $v_s(COO^-)$ of acetate species, respectively [8,35,36]. Furthermore, the band at 1373 cm⁻¹ due to $\delta(C-H)$ and the one at 1081 cm⁻¹ due to $\nu_s(C-O)$ provided additional evidences for the existence of acrylic acid [37]. It is noted that acrylic acid species was detectable even at 150 °C, in spite of its quantity being very rare. At the elevated temperatures, the characteristic bands of acrylic acid became more apparent while that of acrylamide declined slightly; convincingly showing that acrylic acid was obtained through further hydrolysis of acrylamide. Meanwhile, the characteristics of bending bands $[\delta(N-H)]$ of acrylamide were detected at 954 and 981 cm⁻¹ associated with a shoulder at 936 cm⁻¹ attributed to gaseous NH₃ [38]. The transformation from

acrylamide to acrylic acid and ammonia can be described by Eqs. (3) and (4):

$$CH_{2}=CH \qquad O \qquad O \qquad O$$

$$NH_{2}^{-} \qquad CH_{2}=CHC^{-} \qquad NH_{2}^{-}$$

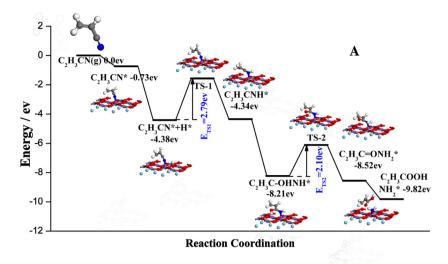
$$Fe^{2+} \qquad Fe^{3+} \qquad Fe^{3+} \qquad Fe^{3+}$$

$$O^{2-} \qquad O^{2-} \qquad (3)$$

$$\begin{array}{c}
O \\
CH_2 = CHC \\
Fe^{3+} \\
O^{2-}
\end{array} + H_2O \longrightarrow \begin{array}{c}
CH_2 = CHCOOH \\
Fe^{3+} \\
Fe^{3+} \\
O^{2-}
\end{array} + Fe^{3+}$$

$$(4)$$

Furthermore, the weak band of 1283 cm⁻¹ appearing at 150 °C was also observed and attributed to the linear nitrite [22], but retained its lower quantity which is consistent with the results obtained from activity test. It is worth noting that the band of linear nitrite shifted lightly toward lower wavenumber of 1265 cm⁻¹ at 300 °C due to a formation of more stable chelating nitrite instead of the linear one [39]. This indicates that molecular vibration of nitrite has been reinforced, to some extent, making nitrite more stable. Two additional bands at 1336 and 1420 cm⁻¹ could be detected which was respectively attributed to the bridging nitrite and ionic nitrate [Fe³⁺(NO₃⁻)₃] species. Subsequently, the characteristic band attributed to $v_{as}(COO^-)$ at 300 °C showed a blue shift from $1540\,\mathrm{cm}^{-1}$ to $1556\,\mathrm{cm}^{-1}$ due to a synergistic effect between acetate and nitrate [38,40]. These results indicate that NH_3 or $-NH_2$ species could be oxidized to adsorbed NO- at relatively high temperatures which is further oxidized to unstable nitrite species, subsequently to more stable nitrate species. The process can be described by Eqs. (5) and (6). However, the intensity of these NO_x



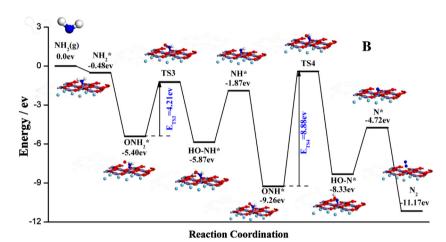


Fig. 4. A, B: Gibbs free energy profile for the reaction to generate acrylic acid and N₂ on LaFeO₃.

species with high oxidation states were never significant, indicating the low yields of possible N_2O , NO, and NO_2 products.

On the basis of above analysis, it gives sufficient explanation for the higher NH $_3$ amount as compared to NO $_x$ amount achieved over LaFeO $_3$ perovskite. It was previously reported that acrylonitrile decomposition over Cu-ZSM-5 proceeds by a hydrolysis of nitrogen-containing intermediates, such as —NCO [7]. However, the noticeable —NCO band was never observed, showing that the formation of —NCO species is impossible as well as its hydrolysis to form NH $_3$ and further oxidation to yield N $_2$ unlikely occur on the bare LaFeO $_3$ perovskite. Accordingly, it is concluded that NH $_3$ or —NH $_2$ was further oxidized at active sites by surface oxygen and two NH $_x$ species were thereafter combined to generate azo-species with the cleavage of N-H bond.

3.3.2. In-situ DRIFTS of catalytic combustion of acrylonitrile over $LaFe_{0.8}Cu_{0.2}O_3$

In the case of LaFe_{0.8}Cu_{0.2}O₃ and exposure under 150 °C, the bands at 1203, 1546, 1601, and 1670 cm $^{-1}$ (see Fig. 3) are attributed to the adsorbed acrylamide species, indicating that Cu corporation into LaFeO3 has some influences on the generation of intermediate species during acrylonitrile catalytic elimination, among which the band at 1670 cm⁻¹ was accordingly attributed the C=C vibrations [ν (C=C)] of acrylamide. Besides, the band at 1639 cm⁻¹ was ascribed to C=O stretching vibration [$v_s(C=O)$], and the bands at 1072, 1432, and 1546 cm⁻¹ belong to $\nu_s(C-0)$, $\nu_s(C00^-)$, and $v_{as}(COO^{-})$ of carboxylic acid species, respectively. However, these characteristic bands are herein not significant especially for C=C vibrations [ν (C=C)] at 1670 cm⁻¹. In comparison of Fig. 2 with Fig. 3, it is noted that the characteristic band of C=C vibrations [ν (C=C)] was clearly detected in the case of LaFeO3 sample between 150 and 300 °C but became minor for LaFe_{0.8}Cu_{0.2}O₃, indicating that the oxidation of anomeric carbon is very weak for LaFeO₃ sample and the existence of C=C is unstable in the presence of Cu because Cu doping promotes the surface oxidation ability at low temperatures. Furthermore, characteristic bands of acrylamide species were not obvious on the surface of LaFe_{0.8}Cu_{0.2}O₃ at 150 °C as compared with those of LaFeO₃, illustrating that acrylamide was not stable and nitrile is likely to be oxidized on LaFe_{0.8}Cu_{0.2}O₃.

As shown in Fig. 3, C=C vibration [ν (C=C)] at 1670 cm⁻¹ is not only apparently observed with an increase of temperature, which

display a fast reaction to form carboxylic acid (-COOH). This oxidation process is described as Eq. (7).

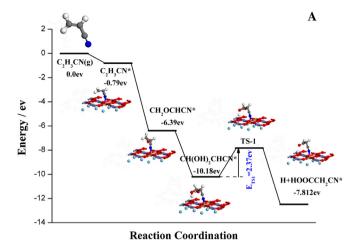
$$\begin{array}{cccc}
CH_2 = CH \\
O_2^{-} & CN^{-} & HOOCCH_2 \\
Fe^{3+} & Cu^{2+} & \longrightarrow & Fe^{2+} & Cu^{2+} \\
O^{2-} & O^{2-} & O^{2-}
\end{array}$$

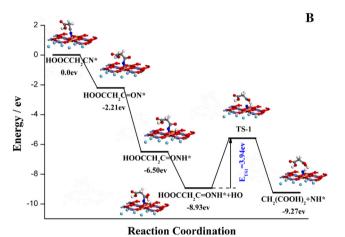
Surprisingly, a sharp new band occurring at $1577\,\mathrm{cm}^{-1}$ was detected when the temperature rose to $200\,^{\circ}\mathrm{C}$. According to the literature reports [41], this band fits perfectly with the adsorbed malonate species, which shows strong vibrations at $1577\,\mathrm{cm}^{-1}$ [$\nu_{as}(\mathrm{COO}^{-})$] and $1432\,\mathrm{cm}^{-1}\,\nu_{s}[(\mathrm{COO}^{-})]$. The latter band consists of contributions from the symmetric stretch vibrations of carboxylate groups and C—H bending modes. This demonstrates that anomeric carbon was simultaneously oxidized to obtain carboxylic acid species, in addition to N-containing group being oxidized. It is the most notable contrast between LaFeO₃ and LaFe_{0.8}Cu_{0.2}O₃ for the corresponding combustion behaviors. N₂ generation could be accomplished via an interaction of two —NH species subsequent with a dehydrogenation process, while the formation of malonate species is described by Eq. (8):

Furthermore, the infrared bands of malonic acid species have become more apparent, and prove the stable existence of malonic acid species at the range of 200–300 $^{\circ}$ C. The band at 1317 cm⁻¹ could be attributed to the monodentate carbonate and its intensity gradually increased accompanying with the rising temperatures. In addition, the IR bands attributed to bending vibration of $\nu_{\delta}(C-H)$ were noticed at 953 and 988 cm⁻¹. In contrast to the findings on LaFeO₃ sample, a new low-intensity band appeared at 2184 cm⁻¹, owing to surface isocyanide (NCO) species [5,40]. Raskó and Kiss previously investigated the adsorption and catalytic reactions of acetonitrile over TiO₂-supported rhodium catalysts knowing that CH₃CN could be first dissociated into CN and successively oxidized into the surface isocyanide (NCO) species [5,42]. Whereas, Liu et al. held another point that nitrates and oxygenates take part in the reaction to form -NCO species [43]. Besides, researchers offer diverse views on the consequent reaction of NCO species. In the case of the SCR of NO_x by C₂H₅OH or C₃H₆ over Cu/Al₂O₃ or Ag/Al_2O_3 , He et al. proposed that NCO reacts with NO + O_2 and even nitrates to yield N₂ [34,36,37,40], while the NCO species was rather stable over Cu/Ti_{0.7}Zr_{0.3}O₂ catalyst in an atmosphere of NO+O₂ [43,44] and then it might be hydrolyzed to form NH₃ and successively reacted with nitrate/nitrite to yield N2. In this study, NCO species were observed 2184 cm⁻¹ and the band intensity increased monotonously as temperature rises, but suddenly decreased at 300 °C. Moreover, an interesting phenomenon could be noted that the bands at 930 and $960\,\mathrm{cm}^{-1}$ attributed to gaseous $\mathrm{NH_3}$ became significant once the characteristic band of NCO decreased, implying that the pathway of NCO hydrolysis to form NH₃ is more credible. The formation of isocyanide and further hydrolysis are described by Eqs. (9) and (10):

$$Fe^{2+} \Box Cu^{2+} + H_2O \longrightarrow Fe^{2+} \Box Cu^{2+} + CO_2$$

$$O^{2-} \qquad (10)$$





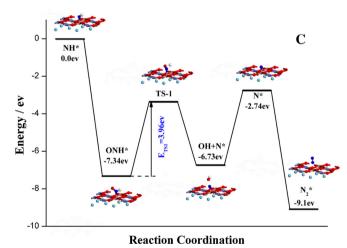
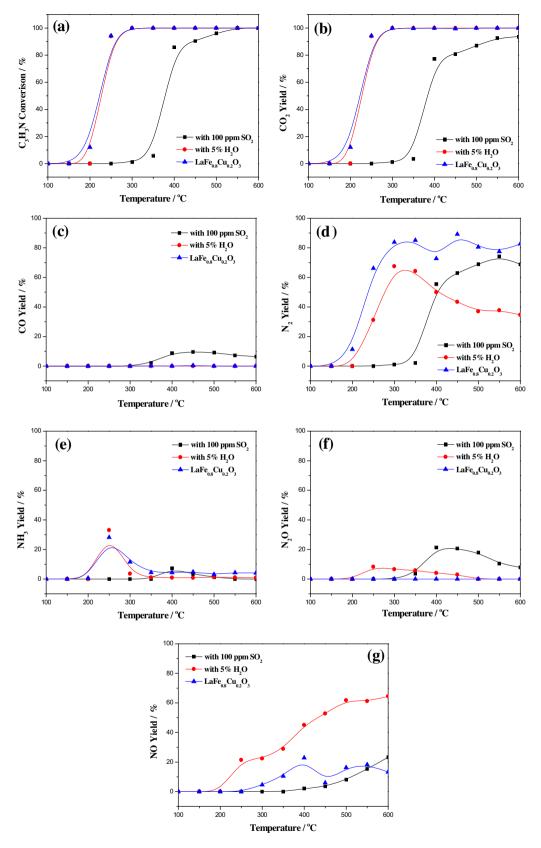


Fig. 5. A B, C: Gibbs free energy profile for the reaction to generate $HOOCCH_2CN$ -Fe, malonic acid species, and N_2 on $LaFe_{0.8}Cu_{0.2}O_3$.

In addition to malonate, small amount of NCO species thought as an intermediate was obtained over LaFe $_{0.8}$ Cu $_{0.2}$ O $_3$, which implies a mechanism obviously different from that related to LaFeO $_3$. However, the intensity of NCO was just minor compared with that of malonate, so the process of NCO hydrolysis might be a side reaction. The bands at 2263, 2337 cm $^{-1}$ were attributed to gaseous CO $_2$ and the intensity of these two bands gradually increased from 150 to 300 °C. It is known that the formed malonic acid species



 $\textbf{Fig. 6}. \text{ The water and sulfur resistance over LaFe}_{0.8} \text{Cu}_{0.2} \text{O}_3 \text{ at the whole temperature range: (a) } C_3 \text{H}_3 \text{N conversion, (b) } \text{CO}_2 \text{ yield, (c) CO yield, (d) } \text{N}_2 \text{ yield, (e) NH}_3 \text{ yield, (f) NP}_2 \text{ yield, (g) NO}_2 \text{ yield, (g) NO}_2 \text{ yield, (g) NO}_3 \text{$

was finally oxidized into CO_2 at the elevated temperatures [36,45]. The weak bands at 1203 and 1601 cm⁻¹ could be attributed to the coordinated NH₃ on Lewis acid sites [32]. The band appear-

ing at $1203\,\mathrm{cm^{-1}}$ for LaFeO $_3$ sample was intensified along with the temperature increase, but there is little information at $1203\,\mathrm{cm^{-1}}$ for LaFeO $_8$ Cu $_0.2$ O $_3$, suggesting NH $_3$ generation over LaFeO $_3$ is more

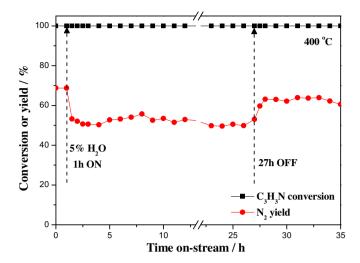


Fig. 7. The H₂O resistance stability over LaFe_{0.8}Cu_{0.2}O₃ with change of time.

easily than that over LaFe $_{0.8}$ Cu $_{0.2}$ O $_3$ at 300 °C. This result is consistent with that obtained from activity measurement. In addition, the bands at 1457 and 1546 cm $^{-1}$ assigned to $\nu_s(\text{COO}^-)$ and $\nu_{as}(\text{COO}^-)$ of carboxylate species were detected again, which explained that the partial oxidation reaction occurred at 150 °C over Cu-doped perovskite. With the temperature rises, a red shift from 1457 to 1432 cm $^{-1}$ together with an overlapping of band at 1546 cm $^{-1}$ with that at 1577 cm $^{-1}$ indicated that abundant carboxylate species were formed. It is worth noting that the area of carboxylate characteristic band achieving at 200–300 °C was larger than that achieving at 150 °C, which seems to demonstrate carboxylate was generated not only at N-end but also at C-end. Likewise, the very weak band of 1270 cm $^{-1}$ achieving at 250 and 300 °C attributed to the chelating nitrite species was also observed [37].

In general, Cu substitution could efficiently improve the transformation of anomeric carbon into carboxylate. Besides, some NCO species were also partly generated at N-end in addition to acrylamide formation. Subsequently, the consumption of the N-containing species including the NCO could be mainly caused by the reaction with $\rm H_2O$, which was considered as two crucial steps to generate $\rm N_2$.

3.4. Mechanism study based on DFT calculation

In order to further verify how acrylonitrile was adsorbed on the surface of Fe-based perovskite, how the intermediate species was formed, and how the final products, especially N₂, was generated during the reaction, DFT calculation was introduced combined with *in-situ* IR results, aiming at giving a more elaborative reaction mechanism.

The possible adsorption modes and adsorption energies were calculated based on the FeO-terminated LaFeO $_3$ because B-site cations are commonly regarded as active centers for the perovskite-type oxides. Acrylonitrile adsorption is illustrated in Section S8 of SI. The calculated adsorption configurations and energies are shown in Fig. S4 and Table S4. In light with DFT calculation, it is proposed that configure A is the most-likely configuration for the adsorbed acrylonitrile existing over LaFeO $_3$ in a manner described by Eq. (1) with an adsorption energy of -0.73 ev.

3.4.1. Formation of acrylic acid over LaFeO₃

To further confirm the generation of acrylic species as evidenced by *in-situ* infrared study, the free energies of the possible intermediates and transition states as well as the reaction pathways were calculated. The results on the Gibbs-free-energy profiles are displayed in Fig. 4A.

As shown in Fig. 4A, acrylonitrile was initially adsorbed on the surface of LaFeO₃ with formation of Fe³⁺-NC structure. Subsequently, Fe³⁺-NC was attacked by H atom from the adsorbed H₂O considering that the reaction process followed a hydrolysis mechanism. Surprisingly, H atom was steadily adsorbed at O-site adjacent to Fe-site, with $E_{ads} = -3.46$ ev. It should surmount an energy barrier of 2.79 ev to obtain C₂H₃CNH⁻-Fe³⁺ species accompanying with an activation of N-terminal species, as formulated by Eq. (11). Additionally, triple bonds of -CN were partly fractured to form -CN- along with a change in bond length from 1.187 to 1.244 Å. And then, attempt to conduct a hydroxylation of C₂H₃C=NH⁻-Fe³⁺ species from adsorbed hydroxyl has been done, finding that -OH was connected with C atom adjacent to N-terminal forming a C_2H_3C -OHNH⁻-Fe³⁺ structure, which is described by Eq. (12). Due to the unstable existence of this structure, H atom of hydroxyl was subsequently transferred to N atom with an energy barrier of 2.79 ev, generating the relatively stable structure of acrylamide $(C_2H_3C=ONH_2^--Fe^{3+})$, in accordance with the formulation by Eq. (2). C=N bond was continually destroyed and the bond length was also stretched to 1.418 Å with forming the C-N single bond which is not stable anymore. Subsequently, this C-N single bond was broken quickly to form unsaturated structure which reacted with the hydroxyl from gas phase to yield acrylic species. Ultimately, acrylic acid was desorbed from the surface of catalyst and subsequently adsorbed upon the other active sites (as depicted by Eq. (3)). The -NH₂ species were still adsorbed at the active sites steadily and further oxidized into N2.

3.4.2. Formation of target product of N_2

As shown in Fig. 4B, -NH2 species was initially adsorbed on the surface of catalyst with energy of 0.48 ev and then reacted with atomic O⁻ to get ONH₂⁻-Fe³⁺ species, associated with $E_{ads} = -5.39$ ev. Subsequently, these species quickly undergo hydrogen redistribution that H atom was connected to N atom linked with O atom, forming HO-NH⁻-Fe³⁺ species. This process should overcome an energy barrier of 4.21 ev. The hydroxyl was immediately desorbed from surface leaving NH⁻-Fe³⁺ species on the surface. Subsequently, another atomic O⁻ reacted with N atom achieving O-NH-Fe³⁺ species, conquering a high energy barrier of 8.88 ev to obtain HO-N⁻-Fe³⁺ species. Finally, the N⁻-Fe³⁺ interacted with another N atom to get the end product of N₂ after hydroxyl was stripped. In the process of N₂ generation, the rate-determining step is N-H bond cleavage accompanied with O-H bond connection. Moreover, NH₃ generation is relatively simple that only interaction with H atom from H₂O dissociation could form NH₃. This explains the easy generation of a large number of gaseous NH₃ over LaFeO₃ sample during the activity test. The process of oxidation from $-\mathrm{NH}_2$ species to N_2 are described in Eqs. (13)–(15).

Table 1Bands observed on LaFeO₃ and LaFe_{0.8}Cu_{0.2}O₃ catalyst during *in-situ* DRIFTS experiments and corresponding surface species and vibrations to which they were assigned.

Samples	Category	Peak location (cm ⁻¹)	Surface species	Vibration	Reference
LaFeO ₃	C-	971	Ethenyl	δ(C—H)	
	containing	1673	Ethylene	$\nu(C=C)$	
		1540, 1441	Acetate	$\nu_{\rm as}({\rm COO^-}), \nu_{\rm s}({\rm COO^-})$	[8,39,40]
		1373	Methyl	$\delta(\text{CH}_3)$	[41]
		1081	Carboxylic acid	$\nu_{\rm s}({\rm C-O})$	[41]
	N-	2231, 2245	Nitrile	$\nu(C = N)$	
	containing	954, 981	Acrylamide	$\delta_{\rm s}({\rm N-H})$	[35]
	_	1203, 1590	Ammonia	$\delta_{as}(NH_3)$	[36,37]
		1283	Linear nitrite		[22]
		1265	Chelating nitrite		[42]
		1420	Bridging nitrite		
		1336	Ionic nitrate		
LaFe _{0.8} Cu _{0.2} O ₃	C-	1670	Ethylene	ν(C=C)	
	containing	1639, 1072, 1432, 1546	Carboxylic acid	$\nu_{s}(C=0), \nu_{s}(COO^{-}), \nu_{s}(COO^{-}), \nu_{as}(C=0)$	
		1577, 1371, 1432,	Malonate	$v_{\rm as}({\rm COO^-}) v_{\rm s}({\rm COO^-})$	[45]
		1317	Monodentate carbonate		
		953, 988		ν _δ (C—H)	
	N-	2184	Isocyanide (NCO)		[5,43]
	containing	1270	Chelating nitrite		[42]

 ν : stretching; δ : bending; s: symmetric, as: asymmetric.

3.4.3. The mechanism occurring over LaFe $_{0.8}$ Cu $_{0.2}$ O $_3$ distinct from that occurring over LaFeO $_3$

Because there are significant differences on the generated intermediate species in in-situ DRIFTS experiments for LaFeO₃ and LaFe_{0.8}Cu_{0.2}O₃, the DFT simulation was further used to explore the diversity in details and explain the promoting effect of Cu doping into perovskite on N₂ yield. The related discussion of acrylonitrile adsorption is illustrated in Section S9 of SI and the optimized geometry structures including bond lengths of Fe-O and Cu-O for LaFe_{0.8}Cu_{0.2}O₃ as well as the calculated energies of acrylonitrile adsorption are listed in Table S5.

Since anomeric carbon has been proved to generate carboxylate easily according to in-situ infrared experiments, we have to initially make sure how anomeric carbon was oxidized to carboxylate before N-terminal oxidation was considered. As shown in Fig. 5A, acrylonitrile molecule was also adsorbed on the surface of LaFe_{0.8}Cu_{0.2}O₃ with formation of Cu²⁺-NC structure. In order to get the carboxylate, atomic oxygen (O^-) from adsorbed molecule oxygen (O_2^-) cleaving the carbon-carbon double bonds was adsorbed at C-C site with $E_{ads} = -5.90$ ev with a H atom connected with another atomic oxygen to form hydroxyl. Moreover, anomeric carbon was attacked by hydroxyl and adsorbed it steadily. Furthermore, H atom from Csite is restructured at O atom forming another hydroxyl. Due to the electronic influence of oxygen, two hydroxyl groups upon a carbon atom are essentially unstable. H atom of hydroxyl was cleavaged from O atom with an energy barrier of 2.37 ev, generating the relatively stable structure HOOCCH2CN—Cu. This process is described by Eq. (16) and (17).

atomic O⁻ was used to attack Cu²⁺-CN⁻ showing that it was adsorbed steadily on C-site, forming C=O double bond. In a similar way, two O atoms were drawn close to nitrile and anomeric carbon. However, it is found that one O atom was adsorbed at N-site and another one stably existed at adjacent Cu-site. The difference paths of adsorbed acrylonitrile reacting with oxygen between LaFeO₃ and LaFe_{0.8}Cu_{0.2}O₃ were illustrated in Fig. 5B. Obviously, the ability for carbonaceous species oxidation of LaFe_{0.8}Cu_{0.2}O₃ is better than that of LaFeO₃. This is because the bond length of Fe-O have been shortened resulting in increasing of oxygen density around Fe-site. The improvement of surface oxygen adsorption can be proposed through the generation of anionic vacancies in the crystal lattice by Cu incorporation, giving an easier oxygen diffusion from the bulk to the surface [12]. Fig. 5B presents the formation process of important intermediate species malonic acid species and NH with surmounting an energy barrier of 3.94 ev. This process is described by Eqs. (18) and (19).

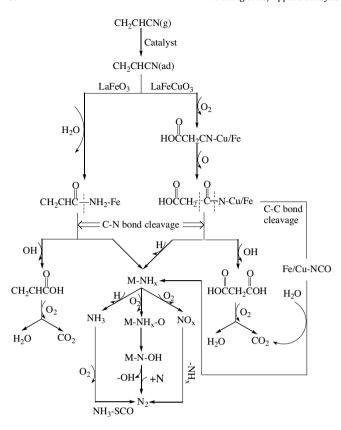
HOOCCH₂ CN O HOOCCH₂ CN
$$Cu^{2+} + Fe^{3+} \longrightarrow Fe^{3+} Cu^{2+} + Fe^{2+}$$
 (18)

Furthermore, Fig. 5C depicted the process of N_2 generation. It should overcome an energy barrier of 3.96 ev to obtain N^* at $LaFe_{0.8}Cu_{0.2}O_3$, which is much lower than the value for $LaFeO_3$. The process is described by Eqs. (20) and (21).

$$Fe^{3+} Cu^{2+} \longrightarrow Fe^{2+} Cu^{2+}$$

$$O^{2-} Cu^{2+}$$

$$O^{2-} (21)$$



Scheme 1. Reaction network for proposed mechanism of the acrylonitrile catalytic combustion reaction over the LaFeO $_3$ and LaFe $_0.8$ Cu $_0.2$ O $_3$ samples.

3.4.4. Reaction network for the mechanism of catalytic combustion of acrylonitrile over LaFeO $_3$ and LaFe $_{0.8}$ Cu $_{0.2}$ O $_3$

The DFT calculations provide sufficient and favorable supporting information for the role of the acrylic acid and malonic acid species respectively forming over LaFeO₃ and LaFe_{0.8}Cu_{0.2}O₃. On the basis of the In-situ DRIFTS study and DFT calculation, an overall mechanism of the catalytic combustion of acrylonitrile for LaFeO₃ and LaFe_{0.8}Cu_{0.2}O₃ is proposed. The main intermediates (appearing in Table 1) are depicted in reaction network of Scheme 1. Acrylonitrile is firstly adsorbed at active sites of LaFeO₃ or LaFe_{0.8}Cu_{0.2}O₃, while two distinct mechanisms to yield N2 are verified due to their different chemical features. It follows hydrolysis-dominating mechanism on the surface of LaFeO₃, in which the adsorbed acrylonitrile is hydrolyzed into acrylamide and C-N bond is further broken to gain acrylic acid and -NH2 species. Acrylic acid is subsequently oxidized to H₂O and CO₂. Simultaneously, -NH₂ is oxidized to final product N2. In the process of N2 generation, the ratedetermining step is the adsorbed O captured H atom from -NH2 to form hydroxyl (-OH). In contrast, it follows oxidation-dominating mechanism over LaFe_{0.8}Cu_{0.2}O₃, in which C-end is initially oxidized into carboxylic acid species and C atom adjacent to N is also oxidized. Next, the formation of N2 over LaFe_{0.8}Cu_{0.2}O₃ is attributed to two separate pathways: (i) the C-N bond cleavage occurred, in which the crucial intermediate of malonic acid species and -NH species are acquired and (ii) C-C bond is fractured to generate small amount of -NCO species. Subsequently, malonic acid species is thereafter oxidized to H₂O and CO₂, and -NH/-NH₂ is transferred into final product N2. In addition, –NCO species can also react with H₂O to yield CO₂ and -NH₂ species. It is worth noting that in the process of N_2 generation for $LaFe_{0.8}Cu_{0.2}O_3$ sample the ratedetermining step is N—H bond fracture and O—H connection again. The presence of Cu can greatly reduce the energy barrier for the

Table 2Adsorption species and site, adsorption energy, and bond lengths involved in single molecule adsorption and influence of H₂O or SO₂ pre-adsorption for reactants and products adsorption on LaFe_{0.8}Cu_{0.2}O₃.

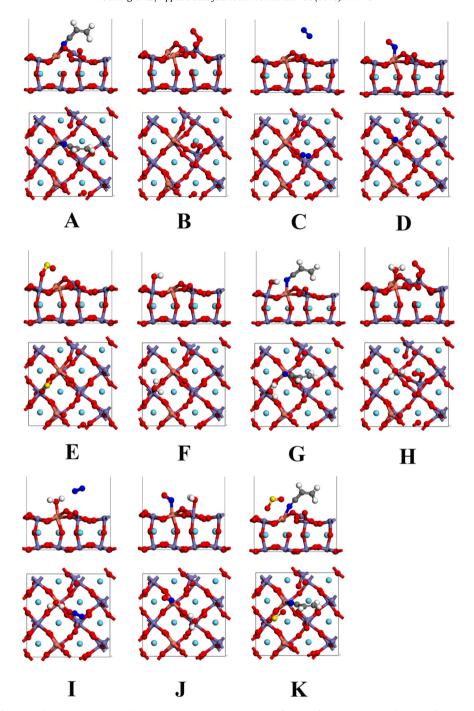
Species	sites	E _{ads} (ev)	Bond lengths (Å)
C ₂ H ₃ CN	Cu – site	-0.842	$d_{Cu-N} = 1.87$
O_2	Fe – site	-1.859	$d_{Fe-O} = 1.76$
N_2	Fe – site	-0.031	$d_{Fe-N} = 3.58$
NO	Cu – site	-1.188	$d_{Cu-N} = 1.83$
SO_2	Fe – site	-0.419	$d_{Fe-O} = 1.96$
H ₂ O	Fe – site	-0.430	$d_{Fe-O} = 2.18$
H ₂ O pre-adsorbed C ₂ H ₃ CN	Cu – site	-0.814	$d_{Cu-N} = 2.09$, $d_{Fe-O} = 2.05$
H ₂ O pre-adsorbed O ₂	Fe – site	-1.944	$d_{Cu-O} = 2.09$, $d_{Fe-O} = 1.76$
H ₂ O pre-adsorbed N ₂	Fe – site	-0.086	$d_{Cu-O} = 2.14$, $d_{Fe-N} = 3.86$
H ₂ O pre-adsorbed NO	Fe – site	-0.769	$d_{Cu-N} = 2.05$, $d_{Fe-O} = 1.85$
SO ₂ pre-adsorbed C ₂ H ₃ CN	Cu – site	-0.435	$d_{Cu-N} = 2.02$, $d_{Fe-O} = 1.83$

transformation from —NH—O to —N—OH, as verified by theoretical calculation, and thus promote the improvement of N₂ yield.

3.5. Resistance to water vapor and sulfur dioxide poisonings

According to the catalytic activities of acrylonitrile (C_2H_3CN) combustion exhibiting in Fig. 1, LaFe_{0.8}Cu_{0.2}O₃ sample was verified to be the optimal catalyst. In order to understand the performance of the catalyst under the real tail-gases conditions, the effect of H₂O and SO₂ on catalytic behaviors during the temperature range of 100-600 °C was investigated. Fig. 6a shows the acrylonitrile conversion at the presence of 5% H₂O or 100 ppm SO₂. Fig. 6b and c present the corresponding yields of C-containing products (CO₂ and CO), and Fig. 6d-g show the yields of N-containing products (N₂, NH₃, N₂O, and NO). As depicted in Fig. 6a, a slightly deactivation of acrylonitrile conversion accompanying with 5% steam addition into the feed at low temperatures (100–300 °C) and a serious drop along with 100 ppm SO₂ introduction at the whole temperature region were observed. The formation of CO₂ product was hardly affected by the presence of H₂O; however, a distinct decline in N₂ yield at 300-600 °C was noticed as well as NO yield was significantly improved due to H2O deactivation. In the presence of 100 ppm SO₂, the decrease of yield of the targeted N₂ was likely ascribed to a decline in number of active centers via coverage by adsorbed sulfurous species (SO_2 , SO_3 , SO_3^{2-} , SO_4^{2-}).

SO₂ poisoning mechanism over perovskite was pointed out by several authors [17,46] that competitive adsorption of SO₂ with reactants as well as the coverage of active sites by surface sulfite and sulfate species may lead to the severe decline of catalytic activity. In our case, the pre-adsorption of SO₂ can lead to a decrease of energy of acrylonitrile adsorption, with a value of -0.435 ev being essentially higher than that of its adsorption alone (-0.842 ev), indicating that acrylonitrile adsorption may be greatly suppressed by SO₂ preadsorption. In addition, SO₃ and SO₄²⁻ species formed during the oxidation process are more stable than SO₂. Combustion activity in the presence of SO₂ was thus inhibited due to a worse acrylonitrile adsorption based on above reasons. In contrast, water adsorption merely resulted in a moderate deactivation. As shown in Table 2, the adsorption energy of H_2O at Cu-top site is -0.430 ev, whereas the adsorption energy of O₂ and acrylonitrile are -1.859 ev and -0.842 ev, respectively, indicating that adsorbed H_2O was less stable than the adsorbed O₂ and C₂H₃CN molecules. Furthermore, the bond strength of acrylonitrile adsorption was slightly weakened after H₂O pre-adsorption. Similar to SO₂ poisoning, the diminution in the number of adsorption sites available for O₂ resulted from H₂O competitive adsorption should also reduce the surface oxidation ability. However, NO yield was improved in the presence of H₂O which is likely to be associated with a "NO formation" mecha-



 $\textbf{Fig. 8.} \ \, \textbf{Side} \ \, \textbf{and} \ \, \textbf{top view of optimized geometries involved in single molecule adsorption and influence of H_2O or SO_2 pre-adsorption for reactants and products adsorption on $LaFe_{0.8}Cu_{0.2}O_3$: (A) C_2H_3CN, (B) O_2, (C) N_2, (D) NO, (E) SO_2, (F) H_2O + C_2H_3CN, (H) H_2O + O_2, (I) H_2O + O_2, (I) H_2O + O_2, (I) H_2O + O_3, (I) H_2O, (I) $$

nism. According to the previous study [47], the adsorption of H_2O may follow Eqs. (22) and (23):

$$Fe^{2+}\Box + H_2O \longrightarrow Fe^{3+}$$

$$Fe^{3+} \qquad (22)$$

$$Fe^{3+} \qquad Fe^{3+} \qquad Fe^{3+} \qquad Fe^{3+} \qquad Fe^{3+} \qquad (23)$$

The adsorption of water can cause an increase of surface hydroxyl. According to Fig. 5C , it would across an energy barrier of 3.96 ev to form adsorbed atomic N. In contrast, it was seen that —ONH could dehydrogenate H atom to obtain the adsorbed NO species. Thereafter, the adjacent hydroxyl capture H atom from —ONH to obtain $\rm H_2O$ molecule by surmounting 1.37 ev (Eq. (24)) which is less than that of forming adsorbed N atom, indicating that the LaFe_{0.8}Cu_{0.2}O_3 surface with high hydroxyl coverage is inclined to acquire H atom generating adsorbed NO. Furthermore, we compared the desorption ability between adsorbed NO with adsorbed $\rm H_2O$. As shown in Table 2, the adsorption energy of individual NO at Fe-site is -1.188 ev while $\rm H_2O$ pre-adsorption can make this value increased up to -0.769 ev, showing that the LaFe_{0.8}Cu_{0.2}O_3 surface

with H_2O adsorption may have stronger NO desorption ability. Furthermore, the N_2 adsorption energy was reduced from -0.031 ev to -0.086 ev due to H_2O pre-adsorption. This might be the reason that N_2 yield declines obviously with 5% H_2O addition.

The reversibility of $\rm H_2O$ deactivation was studied by adding 5% $\rm H_2O$ vapor after the reaction system was stable at 400 °C for 1 h and subsequently removing $\rm H_2O$ at 27 h from the reactant stream as depicted in Fig. 7. All the optimized geometries involved in single molecule adsorption and influence of $\rm H_2O$ or $\rm SO_2$ pre-adsorption for the related adsorption of reactants and products on LaFe0.8Cu0.2O₃ are shown in Fig. 8. The activity of acrylonitrile was marginally affected by the presence of $\rm H_2O$, but about 50–70% decrease of $\rm N_2$ yield occurred. Fortunately, this deactivation caused by $\rm H_2O$ addition can be well recovered by removing steam from the feed. This result shows that the presence of $\rm H_2O$ does not permanently poison the perovskite with its structure being unchanged in the presence of moisture. Consequently, this reversible deactivation caused by $\rm H_2O$ addition is believed to involve the existence of hydroxyl favorable for capturing H atom from —ONH species.

4. Conclusion

In this study, a series of perovskite catalysts with different B-site transition-metals partially substituted by Cu were systematically investigated for the selective catalytic combustion of acrylonitrile, among which LaFe_{0.8}Cu_{0.2}O₃ not only showed the excellent acrylonitrile conversion activity but also presented the best yield towards N2 being a promising candidate used as a catalyst for selective acrylonitrile $\rightarrow N_2$ oxidation. It has been found that Cu-substitution could effectively enhance the redox capacity at low temperatures due to easy Cu²⁺ to Cu⁰ reduction for the perovskite samples and increase the relative concentration of surface adsorption oxygen, which is beneficial for the improvement of acrylonitrile activity at low temperatures. This result suggests that the ability of oxygen adsorption is promoted at LaFe_{0.8}Cu_{0.2}O₃ surface which is attributed to the generation of anionic vacancies in the crystal lattice by Cu incorporation. Furthermore, In-situ DRIFTS investigations combined with DFT calculations were used to elaborately analyze the catalytic mechanism for acrylonitrile combustion, revealing two distinct mechanisms occurred: hydrolysis-dominate mechanism in which the acrylic species steadily existed at the surface of LaFeO3 and oxidationdominating mechanism for LaFe_{0.8}Cu_{0.2}O₃ in which the crucial intermediate of malonic acid species was acquired. Additionally, Cu substitution into LaFeO₃ could greatly reduce energy barrier for the transformation from -NH-O to -N-OH, which is the rate-determining step from -NH_x species to N atom, and further promote the improvement of N2 yield. In addition, LaFe_{0.8}Cu_{0.2}O₃ represented satisfactory resistance to water vapor poisoning.

Appendix A. Supplementary data

Supplementary data associated with this article can be found, in the online version, at http://dx.doi.org/10.1016/j.apcatb.2016.05.025.

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